

Use of a mixture of starch and polyvinylalcohol.

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Inventor(s): NACHTERGAELE WILLY A M; VAN NUFFEL JAN H

Applicant(s):: AMYLUM NV (BE)

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Abstract

50 to 95 parts by weight starch and 5 to 50 parts by weight polyvinyl alcohol with a degree of saponification between 87 and 100% are thoroughly mixed and furthermore the moisture content of the mixture is regulated between 10 and 25 weight %. Subsequently the mixture obtained is subjected to a thermo-mechanical treatment at a temperature situated between 110 and 180 DEG C. During the extrusion the mixture is subjected to shearing forces so that the product obtained when it is dispersed in cold water and subsequently is centrifuged, divides into a watery phase and a coacervate phase without a sediment of undissolved polyvinyl alcohol being formed.

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⑦ Applicant: **MYLUM, N.V.**
Woluwelaan 2
B-1150 Brussel (Sint-Pieters-Woluwe)(BE)

⑧ Inventor: **Nachtergaele, Willy A.M.**
Warandestraat 239
B-9780 Zulte(BE)
Inventor: **Van Nuffel, Jan H.**
Raveschootstraat 8
B-8000 Gent(BE)

⑦ Representative: **Debrabandere, René**
BUREAU DE RYCKER Vereenigde
Octrooibureaux Belge N.V. Arenbergstraat
13
B-2000 Antwerpen(BE)

⑨ Procedure for the manufacture of a mixture of starch and polyvinyl alcohol and thus manufactured mixture.

⑨ 50 to 95 parts by weight starch and 5 to 50 parts by weight polyvinyl alcohol with a degree of saponification between 87 and 100% are thoroughly mixed and furthermore the moisture content of the mixture is regulated between 10 and 25 weight %. Subsequently the mixture obtained is subjected to a thermo-mechanical treatment at a temperature situated between 110 and 180° C. During the extrusion the mixture is subjected to shearing forces so that the product obtained when it is dispersed in cold water and subsequently is centrifuged, divides into a watery phase and a coacervate phase without a sediment of undissolved polyvinyl alcohol being formed.

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Procedure for the manufacture of a mixture of starch and polyvinyl alcohol and thus manufactured mixture

The invention relates to a procedure for the manufacture of a mixture of starch polyvinyl alcohol.

It is known that polyvinyl alcohol in different applications such as adhesives, sizing agent for threads, water dissolvable films and paper coating, exercises a positive influence on the functional properties of the prepared products.

5 The polyvinyl alcohol employed can moreover vary in properties depending on the application. These properties are determined by the degree of hydrolysis and the molecular weight of the product.

In most cases the polyvinyl alcohol needs to be heated sufficiently long in order to bring the product completely into solution.

Furthermore it frequently occurs that polyvinyl alcohol is employed in combination with starch deriva-
10 tives which are soluble or dispersible in cold water.

This is among others the case in the paper coating compositions in which in practice mixtures of starch and polyvinyl alcohol are applied.

Such mixtures exert, in the presence of optical whiteners, an advantageous influence on the whiteness of the paper. Moreover the starch as a solution or otherwise is added to the size of whiteners. However a
15 polyvinyl dispersion must first be manufactured which is then heated in order to dissolve the polyvinyl alcohol.

The starch can also be added directly in dry form to the size of optical whiteners. In the paper coating sector for that matter it is the trend to change over to superior dry material coatings.

The addition of a modified starch in dry form to a pigment size, with the intention of raising the dry
20 material content of the coating composition, was already described in US-A-4 425 452. This method offers as advantage that during the drying of the coated paper less moisture needs to be evaporated, which results in a more economical procedure. According to this patent no use is made however of polyvinyl alcohol.

In the above mentioned application but also in many other applications it would thus be very
25 advantageous that the polyvinyl alcohol would be very quickly soluble in cold water whereby then for example for the manufacture of a paper coating the polyvinyl alcohol could also be added directly in dry form to the pigment slurry. On the one hand therefore the coating installation would be simplified because no solution and heating installation for the starch and the polyvinyl alcohol are necessary. On the other hand a coating agent with a higher dry material content would be obtained through which during the drying of the
30 coated paper less energy needs to be employed in order to evaporate the superfluous moisture and/or through which the speed of the coater can be increased.

A cold soluble polyvinyl alcohol, whether or not in combination with an starch or a derivative thereof, is nevertheless not yet known.

The purpose of the invention now is to provide a procedure for the manufacture of a mixture of starch
35 and polyvinyl alcohol whereby a mixture is obtained that is soluble in cold water.

For this purpose 50 to 95 parts by weight starch and 5 to 50 parts by weight polyvinyl alcohol are thoroughly mixed, furthermore the moisture content of the mixture is regulated between 10 and 25 weight % and subsequently the mixture is subjected to a thermomechanical treatment at a temperature situated
40 between 110 and 180 °C, with which treatment this mixture is subjected to shearing forces such that the product obtained, when it is dispersed in cold water and subsequently centrifuged, divides into a watery phase and a coacervate phase without a third phase consisting of a sediment of undissolved polyvinyl alcohol being formed.

In a particular embodiment of the procedure a continuous extrusion is performed as thermo-mechanical treatment.

45 In a notable embodiment of the invention the moisture content is regulated between 12 and 20 weight % during the mixing of the starch and the polyvinyl alcohol.

In a functional embodiment of the invention a polyvinyl alcohol with a degree of saponification between 87 and 100% is employed.

In paper coating strongly saponified polyvinyl alcohol is preferably applied.

50 The starch employed can be a natural or modified starch. The modified starch can be etherified or esterified and/or oxidatively, by acid or enzymatically broken down.

A granular etherified starch is preferably employed.

In another embodiment of the invention an acid is added to the mixture in order further to break down the starch.

The invention also relates to a mixture of starch and polyvinyl alcohol obtained according to the procedure according to one of the aforementioned embodiments.

Other details and advantages on the invention will appear from the following description of a procedure for the manufacture of a mixture of starch and polyvinyl alcohol and of a thus manufactured mixture, according to the invention; this description is only given as an example and does not restrict the invention.

For the manufacture of a mixture of starch and polyvinyl alcohol according to the invention, 50 to 95 and preferably 85 to 90 parts by weight starch and 5 to 50 and preferably 10 to 15 parts by weight polyvinyl alcohol are thoroughly mixed.

The polyvinyl alcohol has preferably a minimum degree of saponification of 87%. This degree of saponification can go to 100% and particularly for use in paper coating strongly saponified polyvinyl alcohol is preferably employed.

The starch can be natural or modified.

The modified starch can be etherified or esterified and/or be oxidatively, by acid or enzymatically broken down. A granular etherified starch is preferably employed.

The moisture content of the mixture is regulated between 10 and 20 weight %, preferably between 12 and 20 weight % and best between 14 and 18 weight %.

The mixture obtained is subjected to a thermo-mechanical treatment at a temperature situated between 110 and 180 °C.

During this treatment the mixture is subjected to a shearing force so that the product obtained, when it is dispersed in cold water and subsequently centrifuged, divides into a watery phase and a coacervate phase without a third phase consisting of a sediment of undissolved polyvinyl alcohol being formed.

A similar phase would be formed without or without sufficient thermo-mechanical treatment.

A suitable thermo-mechanical treatment is a continuous extrusion.

This extrusion can be performed in an extrusion apparatus that contains a cylinder with one or more rotating screws which give a buildup of pressure in the mixture, whereby the mixture present melts through the internal heat which is released and/or through externally supplied heat.

The melted mixture is then transported by means of the screw or the screws through the pressure cylinder toward the extremity of the extrusion apparatus, whereby the mixture is subjected to the shearing forces. At the extremity of the pressure chamber there are one or more openings through which the mixture is pressed outward.

A suitable extrusion apparatus is for example an apparatus found on the market of the type BUSS-PR 46. Such an extruder has a capacity of 18 kg of product per hour and has a length diameter ratio of 7. The extruder contains two screws with a diameter of 46 mm, namely a dosing screw which rotates at 13 revolutions per minute and an extrusion screw which rotates at 97 revolutions per minute. The time the mixture stays there amounts to 10 to 20 seconds at a temperature of between 130 and 150 °C and a pressure of between 5 and 10 kg per cm².

Other extruders, for example of the type CREUSOT-LOIRE can likewise be employed subject to the adjustment of the reaction conditions to the characteristics of the apparatus in order to obtain the desired shearing forces.

To a mixture an acid can possibly be added in order further to break down the starch. The added amount of acid is preferably selected so that the pH of a 10% suspension of the mixture is situated between 2 and 2.5.

It is surprisingly determined that with use of the extruded mixtures the polyvinyl alcohol present dissolves very well and very quickly in cold water too.

In this way there is a clear difference to be observed in the dissolving speed between polyvinyl alcohol with a low degree of saponification, which is also considered as soluble in cold water, and extruded mixtures of starch and such a polyvinyl alcohol. The difference in dissolving speed is still much more clearly to be observed when strongly or completely saponified or hydrolized polyvinyl alcohol is compared with an extruded polyvinyl alcohol on the basis of starch and such a polyvinyl alcohol.

The extruded mixtures obtained are extremely useful as a binder in coating compositions for the coating of paper. These mixtures can be added in dry form to the pigment slurry, whereby the moisture content of the mixture decreases, which of course is advantageous.

The dry material content of the thus prepared coating composition can moreover be increased with 2 to 4 weight %, which results in a decrease of 7 to 14 weight % of the moisture that needs to be evaporated afterward.

Furthermore it was surprisingly also determined that the application of the extruded mixtures according to the invention as binder in coating compositions gave a significantly greater whiteness to the treated paper than the corresponding non-extruded mixtures. These non-extruded mixtures have to be boiled up

beforehand. It is clear that there is question here of a synergistic effect.

Also films on the basis of extruded mixtures of starch and polyvinyl alcohol show interesting properties, such as a greater tensile strength and breaking length.

The invention will be further explained hereafter with the help of some examples.

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Examples 1 through 5

25 kg of etherified starch, brought onto the market by the depositor under the name of AMYLUM A2, are placed in a mixer and stirred for 5 minutes.

After that the moisture content and pH are determined.

To the starch that has a moisture content of 13.2%, is then added an amount of completely hydrolized (98%) polyvinyl alcohol with low viscosity, obtainable on the market under the name of AIRVOL 107^m of Air Products in the ratio according to the following table 1.

15 The whole is further homogenized and is subsequently mixed with the necessary amount of demineralized water in order to obtain the desired moisture content according to table 1.

Finally the homogenized mixture is measured into doses by means of a dosing screw in an extrusion apparatus of the type CREUSOT-LOIRE EXTRUDER. The mixture is extruded under the extrusion conditions according to the following table 1. In this H.S. indicates a screw with kneading elements and L.S. a standard screw.

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After extrusion the mixture obtained is finely, ground.

table 1

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example	1	2	3	4	5
Composition mixture					
starch	90	90	50	50	90
PVA	10	10	50	50	10
moisture	20	12	20	12	20
extrusion conditions					
T °C	110	180	110	180	110
rotation speed screw (rpm)	100	150	150	100	100
configuration	H.S.	L.S.	H.S.	L.S.	L.S.

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Examples 6 through 8

The procedure according to examples 1 through 5 is repeated but with the composition of the mixtures and the extrusion conditions as in the following table 2, whereby moreover together with the demineralized water for the adjustment of the moisture content also 4 weight % concentrated sulfuric acid, calculated on the amount of starch, is added.

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After the extrusion sodium bicarbonate is added to the extruded mixture in order to neutralize the acid present.

Example 8 is only taken for comparison since there is no PVA present and therefore falls outside of the invention.

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table 2

Example	6	7	8
Composition mixture			
starch	90	90	100
PVA	10	10	-
moisture	12	15	15
extrusion conditions			
T ° C	110	130	130
rotation speed screw (rpm)	150	100	100
screw configuration	H.S.	L.S.	L.S.
(H.S. is a screw with kneading elements and L.S. a standard screw).			

Examples 9 and 10

The procedure according to examples 6 through 8 is repeated but with the composition of the mixtures and the extrusion conditions as in the following table 3 and furthermore with another type of polyvinyl alcohol, namely an only partially hydrolized (88-90%) polyvinyl alcohol with low viscosity that is obtainable on the market under the name of AIRVOL 203 ⁽¹⁾ of Air Products.

table 3

Example	9	10
Composition mixture		
starch	50	90
PVA	50	10
moisture	16	16
extrusion conditions		
T ° C	130	130
rotation speed screw (rpm)	100	100
screw configuration	L.S.	L.S. (standard screw)

Results

The extruded mixtures obtained according to the examples described above were dispersed in cold water, in a concentration of 5 weight % and stirred for 3 minutes. The dispersed mixtures were subsequently centrifuged for 10 minutes at 3000 revolution per minute.

For comparison the following mixtures which were not prepared according to the invention and thus were not extruded, were likewise dispersed and centrifuged:

Example 11

90 parts by weight starch AMYLUM A2 prepared according to the procedure from example 8 with a moisture content of 15% and 10 parts by weight polyvinyl alcohol, AIRVOL 107 ⁽¹⁾.

Example 12

50 parts by weight starch AMYLUM A2 prepared according to the procedure from example 8 with a moisture content of 15% and 50 parts by weight polyvinyl alcohol AIRVOL 107 ⁽¹⁾.

Example 13

90 parts by weight starch AMYLUM A2 prepared according to the procedure from example 8 with a moisture content of 15% and 10 parts by weight polyvinyl alcohol AIRVOL 203 ⁽¹⁾.

In table 4 shown hereafter the viscosities of the dispersions and the centrifuge results are shown.

The distribution of the various phases are shown in percentages.

table 4

Example	Viscosity in mP	Moisture %	Gel %	Sediment %
1	98	52	48	-
2	92	29	41	-
3	38	79	21	-
4	42	88	12	-
5	82	50	50	-
6	30	95	5	-
7	20	99	1	-
8	20	99	1	-
9	32	98	2	-
10	26	99	1	-
11	20	97	1	2
12	20	92	1	7
13	23	98	1	1

An additional test was performed on the layer of viscous mixtures in order to verify to what extent the polyvinyl alcohol present was dissolved.

During this the sample material was dispersed in cold water under violent stirring. The concentration of the dispersions amounted to 28% dry material. The dispersions obtained were then filtered through a 53 micron sieve. The residue on the sieve was then dried and weighed. The residue was expressed as a percentage of the amount of dry material used. The residual polyvinyl alcohol content was then determined from the difference with a reference sample, which contained no polyvinyl alcohol. The results are shown in the following table 5.

table 5

	residue	residual polyvinyl alcohol
6	0.7%	2.7%
7	0.8%	3.9%
10	0.56%	1.3%
11	8.45%	80.2%
13	1.35%	9.0%
reference	0.43%	-

The residual polyvinyl alcohol was expressed as a percentage of the polyvinyl alcohol present, which is

not dissolved.

From table 5 it clearly appears that the polyvinyl alcohol present with the examples according to the invention is practically completely dissolved. In the case that partially hydrolized polyvinyl alcohol was employed it appears that here also the solubility is greatly improved.

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Applications.

"Coating" compositions were produced by means of products according to the invention and compared with known compositions.

Moreover the dry material and the viscosity of the "coating" mixture, as well as the dry material after dilution of the pigment size were determined at 1000 mP. After treatment of the paper with this composition the whiteness was measured with the assistance of a Hunterlab apparatus.

The products of the invention were added to the "coating-premix" in dry form. In the other cases the binder or co-binder had to be dissolved beforehand with exception of the extruded starch from example 8.

In the following examples the following precoating composition was employed:

pigment :

80 parts calcium carbonate (Hydrocarb 90) ⁽¹⁾

20 parts China clay (Amazon 88) ⁽¹⁾

20 binder :

8 parts styrene butadiene latex (DL 885) ⁽¹⁾

additive :

1 part Urecoll ⁽¹⁾

1 part calcium stearate

25 1.5 parts optical whitener (Blancophor P)

This size has a dry material content of 72.0%.

The added materials and the results obtained are shown in the following table 6:

table 6

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composition	binder	parts	%d.m. (1)	viscosity mP	%d.m. (2)
I latex	2	69.0	2450	65.0	90.9
CMC	1				
II latex	2	67.4	920	67.4	90.8
AIRVOL 107 ⁽¹⁾	1				
III from ex. 8	4	72.5	3000	66.3	89.7
IV from ex. 7	4	72.5	1840	69.3	92.2
V from ex.10	4	72.5	2560	68.2	91.4
VI from ex.11	4	70.5	2500	66.7	90.8
VII from ex.13	4	70.5	2200	67.0	90.9

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(1) before dilution.

(2) after dilution to 1000 mP.

From the above table it therefore clearly appears that in the case of the compositions IV and V "coating" mixtures are obtained with a distinctly higher dry material, when compared with the compositions I and II.

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In addition to this the greater whiteness for paper "coated" with this composition is striking; a gain of 0.5 to 1% in whiteness is considered as a great advantage in the paper industry.

Another application exists in manufacturing water soluble films.

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A water soluble film manufactured on the basis of the mixture of starch and polyvinyl alcohol manufactured according to the above mentioned example 2 was compared with a pure polyvinyl alcohol film (polyvinyl alcohol AIRVOL 203⁽¹⁾) and with a film on the basis of a mixture with the same composition as in example 2 but without the extrusion according to the invention.

The mixture of the pure polyvinyl alcohol was boiled up beforehand. The composition according to example 2 was stirred up in cold water and used as such.

The concentration of the solution amounted to 10%.

The spread out solutions were left to dry in the air.

The tensile strength, the breaking length and the elongation capacity of the films obtained is shown in the following table 7.

table 7

	film thickness (mm)	weight (g/m ²)	tensile strength (daN)	breaking length (km)	elongation (mm)
(1)	0.063	74.18	2.23	2.00	21.7
ex. 2	0.056	78.25	3.21	2.80	1.5
mixture	0.062	86.25	2.04	1.60	1.7

(1) AIRVOL 203^(r)

The invention is in no way restricted to the embodiments described above and within the scope of the patent application many changes can be applied to the described embodiments, among others regarding the choice of the raw materials and the apparatus employed.

Claims

1. Procedure for the manufacture of a mixture of starch and polyvinyl alcohol, characterized in that 50 to 95 parts by weight starch and 5 to 50 parts by weight polyvinyl alcohol are thoroughly mixed, furthermore the moisture content of the mixture is regulated between 10 and 25 weight % and subsequently the mixture obtained is subjected to a thermo-mechanical treatment at a temperature situated between 110 and 180 °C, with which treatment this mixture is subjected to shearing forces such that the product obtained, when it is dispersed in cold water and subsequently centrifuged, divides into a watery phase and a coacervate phase without a third phase consisting of a sediment of undissolved polyvinyl alcohol being formed.

2. Procedure according to claim 1, characterized in that a continuous extrusion is performed as thermo-mechanical treatment.

3. Procedure according to one of the claims 1 and 2, characterized in that the moisture content is regulated between 12 and 20 weight % during the mixing of the starch and the polyvinyl alcohol.

4. Procedure according to claim 3, characterized in that the moisture content is regulated between 14 and 18 weight % during the mixing of the starch and the polyvinyl alcohol.

5. Procedure according to one of the claims 1 through 4, characterized in that a polyvinyl alcohol with a degree of saponification between 87 and 100% is employed.

6. Procedure according to one of the claims 1 through 5, characterized in that a mixture is manufactured of 85 to 90 parts by weight starch and 10 to 15 parts by weight polyvinyl alcohol.

7. Procedure according to one of the claims 1 through 6, characterized in that as starch a granular etherified starch is employed

8. Procedure according to one of the claims 1 through 7, characterized in that an acid is added to the mixture in order further to break down the starch.

9. Procedure according to claim 8, characterized in that the acid is so selected that the pH of a 10% suspension of the mixture is situated between 2 and 2.5.